

#1. Consider the following steady, two dimensional velocity field:

$$V = (u, v) = (0.5 + 1.2x)\mathbf{i} + (-2.0 - 1.2y)\mathbf{j}$$

Is there a stagnation point in this flow field? If so where is it?

Solve: At stagnation point

$$u=0 \Rightarrow 0.5 + 1.2x = 0 \Rightarrow x = -0.5/1.2 = -0.417$$

$$v=0 \Rightarrow -2.0 - 1.2y = 0 \Rightarrow y = -1.67$$

So, the stagnation point is $(-0.417, -1.67)$.

#2. A steady, incompressible, two dimensional velocity field is given by the following components in the x-y plane:

$$u = 1.1 + 2.8x + 0.65y, v = 0.98 - 2.1x - 2.8y$$

Calculate the acceleration field and calculate the acceleration the fluid experiences at point $(x, y) = (-2, 3)$.

Solve: $a = \frac{\partial \vec{v}}{\partial t} + (\vec{v} \cdot \nabla) \vec{v} = u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y}$

$$u \frac{\partial v}{\partial x} = u \frac{\partial}{\partial x} [(1.1 + 2.8x + 0.65y)\vec{i} + (0.98 - 2.1x - 2.8y)\vec{j}]$$

$$= u (2.8\vec{i} - 2.1\vec{j})$$

$$v \frac{\partial v}{\partial y} = v \frac{\partial}{\partial y} [(1.1 + 2.8x + 0.65y)\vec{i} + (0.98 - 2.1x - 2.8y)\vec{j}]$$

$$= v (0.65\vec{i} - 2.8\vec{j})$$

$$\text{So, } a = (1.1 + 2.8x + 0.65y)(2.8\vec{i} - 2.1\vec{j}) + (0.98 - 2.1x - 2.8y)(0.65\vec{i} - 2.8\vec{j})$$

$$= (3.717 + 6.475x)\vec{i} - (5.054 - 6.495y)\vec{j}$$

At point $(x, y) = (-2, 3)$

$$a = [3.717 + (6.475)(-2)]\vec{i} - [5.054 - (6.495)(3)]\vec{j}$$

$$= -9.233\vec{i} + 14.37\vec{j}$$

#3. The temperature T , in a long tunnel is known to vary approximately as $T = T_0 - \alpha e^{-x/L} \sin(2\pi t/\tau)$, where T_0 , α , L and τ are constants, and x is measured from the entrance. A fluid moves into the tunnel with a constant speed, U . Obtain an expression for the rate of change of temperature experienced by the fluid.

Solve: Given: $T = T_0 - \alpha e^{-x/L} \sin(2\pi t/\tau)$

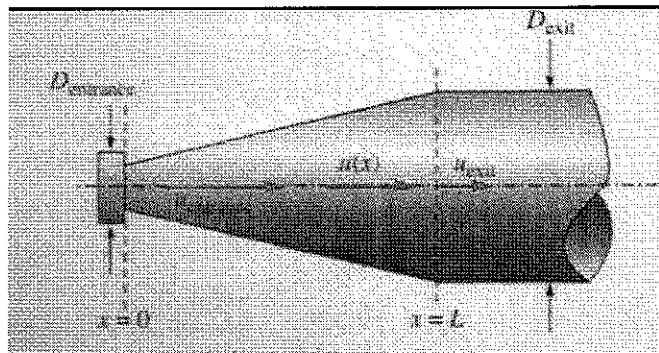
$$\frac{DT}{Dt} = \frac{\partial T}{\partial t} + (\mathbf{V} \cdot \nabla) T$$

$$\frac{\partial T}{\partial t} = 0 - \alpha e^{-x/L} \frac{2\pi}{\tau} \cos\left(\frac{2\pi t}{\tau}\right) = -\frac{2\pi \alpha}{\tau} e^{-x/L} \cos\left(\frac{2\pi t}{\tau}\right)$$

$$\begin{aligned} (\mathbf{V} \cdot \nabla) T &= U \frac{\partial T}{\partial x} = U \frac{\partial}{\partial x} \left[T_0 - \alpha e^{-x/L} \sin\left(\frac{2\pi t}{\tau}\right) \right] \\ &= \frac{U \alpha}{L} e^{-x/L} \sin\left(\frac{2\pi t}{\tau}\right) \end{aligned}$$

$$\begin{aligned} \text{So, } \frac{DT}{Dt} &= -\frac{2\pi \alpha}{\tau} e^{-x/L} \cos\left(\frac{2\pi t}{\tau}\right) + \frac{U \alpha}{L} e^{-x/L} \sin\left(\frac{2\pi t}{\tau}\right) \\ &= \alpha e^{-x/L} \left[\frac{U}{L} \sin\left(\frac{2\pi t}{\tau}\right) - \frac{2\pi}{\tau} \cos\left(\frac{2\pi t}{\tau}\right) \right] \end{aligned}$$

#4. Consider steady flow of air through the diffuser of a wind tunnel as shown. Along the centerline of the diffuser, the air speed decreases from $u_{entrance}$ to u_{exit} as sketched. Measurements reveal that the centerline airspeed decreases parabolically through the diffuser. Write an equation for the centerline speed $u(x)$ and the fluid acceleration $a(x)$ along the centerline based on the parameters given, $x = 0$ to $x = L$. For $L = 2.0 \text{ m}$, $u_{entrance} = 30 \text{ m/s}$ and $u_{exit} = 5.0 \text{ m/s}$, calculate the acceleration at $x = 0$ and $x = 1.0 \text{ m}$.



Solve: According to centerline airspeed decrease parabolically,

$$u(x) = u_{entrance} - ax^2$$

$$\text{At } x=0, \quad u = u_{entrance} = 30 \text{ m/s}$$

$$x=L=2.0 \text{ m}, \quad u = u_{exit} = 5.0 \text{ m/s}$$

$$\therefore 5 = 30 - aL^2 = 30 - 4a \Rightarrow a = \frac{25}{4} = 6.25$$

$$\text{So } u(x) = 30 - 6.25x^2$$

$$a = u \frac{\partial v}{\partial x} = (30 - 6.25x^2)(-12.5x)$$

$$\text{At } x=0, \quad a=0$$

$$x=1.0 \text{ m}, \quad a = (30 - 6.25)(-12.5)$$

$$= -296.875 \text{ m/s}^2$$

#5. After discarding any constants of integration, determine the appropriate value of the unknown velocities w or v that satisfy the equation of three-dimensional incompressible continuity for

$$(a) u = x^2 yz \quad v = -y^2 x$$

$$(b) u = x^2 + 3z^2 x \quad w = -z^3 + y^2$$

Solve: three-dimensional incompressible continuity:

$$0 = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

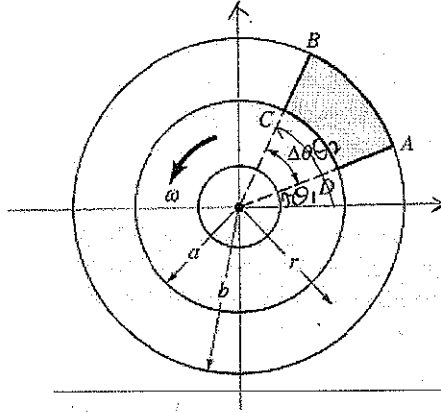
$$(a) \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \Rightarrow 2xyz - 2xy + \frac{\partial w}{\partial z} = 0$$

$$\Rightarrow w = \int (2xyz - 2xy) dz = xyz^2 - 2xy z$$

$$(b) \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \Rightarrow 2x + 3z^2 + \frac{\partial v}{\partial y} - 3z^2 = 0$$

$$\Rightarrow v = \int -2x dy = -2xy$$

#6. The forced vortex shown below is composed of streamlines that are concentric circles. The velocity is given by $v_\theta = \omega r$ and $v_r = 0$ where ω is the constant angular velocity of the vortex. Is this flow irrotational? Determine the circulation around path $ABCD$.



Solve:

$$\Gamma = \oint_{ABCD} \vec{v} \cdot d\vec{s} = \int_{AB} v_\theta b d\theta + \int_{BC} v_r dr + \int_{CD} v_\theta a d\theta + \int_{DA} v_r dr$$

Since $v_r = 0$, $v_\theta = \omega r$

$$\begin{aligned} \Gamma &= \int_{\theta_1}^{\theta_2} \omega b^2 d\theta + \int_{\theta_2}^{\theta_1} \omega a^2 d\theta \\ &= \omega b^2 (\theta_2 - \theta_1) + \omega a^2 (\theta_1 - \theta_2) \\ &= \omega \Delta\theta (b^2 - a^2) \end{aligned}$$

\therefore This flow is not irrotational.

#7. A two-dimensional flow is defined by

$$u = -\frac{Ky}{x^2 + y^2}, \quad v = +\frac{Kx}{x^2 + y^2}$$

Where $K = \text{constant}$. Is this flow incompressible and irrotational? If so, find its velocity potential and stream function. Plot a few potential and stream lines, and interpret the flow pattern.

Solve: For incompressible flow, $\nabla \cdot \vec{V} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = \frac{2Kxy}{(x^2 + y^2)^2} - \frac{2Kxy}{(x^2 + y^2)^2} = 0$$

\therefore this flow is incompressible.

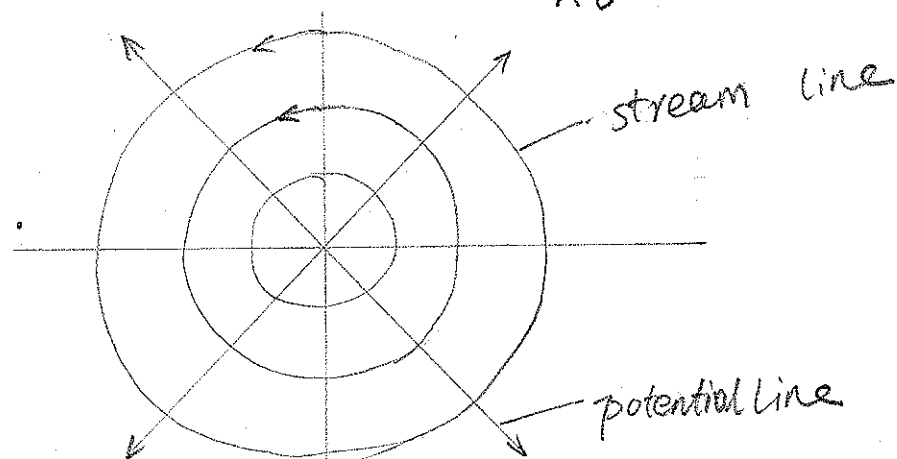
For irrotational flow, $\nabla \times \vec{V} = \frac{\partial u}{\partial y} - \frac{\partial v}{\partial x} = 0$

$$\frac{\partial u}{\partial y} - \frac{\partial v}{\partial x} = \frac{2Ky^2 - K(x^2 + y^2)}{(x^2 + y^2)^2} + \frac{2Kx^2 - K(x^2 + y^2)}{(x^2 + y^2)^2}$$

$$= 0$$

\therefore this flow is irrotational.

$$u = \frac{\partial \phi}{\partial x} = -\frac{Ky}{x^2 + y^2} \Rightarrow \phi = \int -\frac{Ky}{x^2 + y^2} dx = -K \tan^{-1}\left(\frac{x}{y}\right) = K\theta$$



Flow pattern : source

#8. A two-dimensional incompressible flow field is defined by the velocity components

$$u = 2V\left(\frac{x}{L} - \frac{y}{L}\right) \quad v = -2V\frac{y}{L}$$

where V and L are constants. If they exist, find the stream function and velocity potential.

Solve: $\nabla \cdot \vec{v} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = \frac{2V}{L} - \frac{2V}{L} = 0$

\therefore satisfy continuity means ψ exist.

$$\nabla \times \vec{v} = \frac{\partial u}{\partial y} - \frac{\partial v}{\partial x} = -\frac{2V}{L} - 0 = -\frac{2V}{L} \neq 0$$

\therefore not satisfy irrotational means ϕ does not exist.

According to: $\frac{\partial \psi}{\partial y} = u = 2V\left(\frac{x}{L} - \frac{y}{L}\right)$

$$\Rightarrow \psi = \int 2V\left(\frac{x}{L} - \frac{y}{L}\right) dy = \frac{2Vxy}{L} - \frac{Vy^2}{L} + C(x)$$

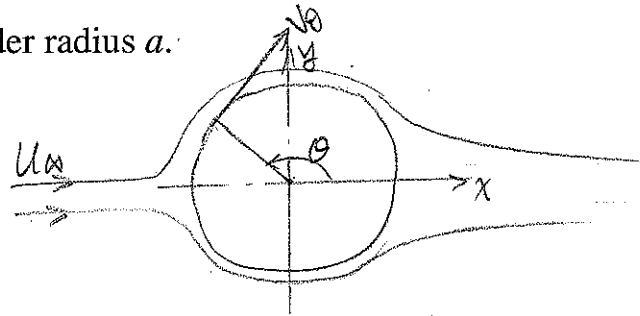
According to: $\frac{\partial \psi}{\partial x} = -v = 2V\frac{y}{L}$

$$\Rightarrow \psi = \int 2V\frac{y}{L} dx = 2V\frac{xy}{L} + C(y)$$

$$\text{So, } \psi = \frac{2Vxy}{L} - \frac{Vy^2}{L} + C$$

#9. A circular cylinder is fitted with two surface-mounted pressure sensors, to measure p_a at $\theta=180^\circ$ and p_b at $\theta=105^\circ$. The intention is to use the cylinder as a stream velocimeter. Using potential flow theory, derive a formula for estimating U_∞ in terms of p_a, p_b, ρ , and the cylinder radius a .

Solve: Tangential Velocity on the surface of circular cylinder in free stream velocity U_∞ is



$$V_\theta = -2U_\infty \sin\theta$$

Apply Bernoulli equation between free stream and point a

$$\theta = 180^\circ,$$

$$p_\infty + \frac{1}{2}\rho U_\infty^2 = p_a + \frac{1}{2}\rho U_a^2 = p_a + \frac{1}{2}\rho(-2U_\infty \sin(180^\circ))^2$$

$$\Rightarrow p_\infty = p_a - \frac{1}{2}\rho U_\infty^2 \quad (1)$$

Apply Bernoulli equation between free stream and point b

$$\theta = 105^\circ$$

$$p_\infty + \frac{1}{2}\rho U_\infty^2 = p_b + \frac{1}{2}\rho U_b^2 = p_b + \frac{1}{2}\rho(-2U_\infty \sin(105^\circ))^2$$

$$\Rightarrow p_\infty = p_b + 2\rho U_\infty^2 \sin^2(105^\circ) - \frac{1}{2}\rho U_\infty^2 \quad (2)$$

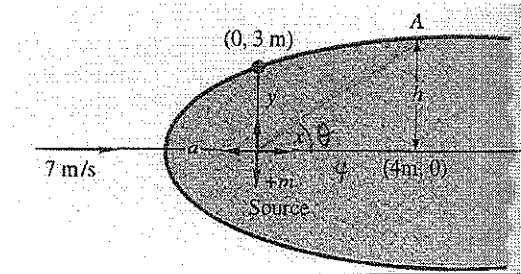
According to equation (1) & (2).

$$p_a - \frac{1}{2}\rho U_\infty^2 = p_b + 2\rho U_\infty^2 \sin^2(105^\circ) - \frac{1}{2}\rho U_\infty^2$$

$$\Rightarrow p_a - p_b = 2\rho U_\infty^2 \sin^2(105^\circ)$$

$$\Rightarrow U_\infty = \sqrt{\frac{p_a - p_b}{2\rho \sin^2(105^\circ)}}$$

#10. A Rankine half-body is formed as shown. For the stream velocity and body dimension shown, compute (a) the source strength m in m^2/s , (b) the distance a , (c) the distance h , and (d) the velocity magnitude at point A.



Solve: for Rankine half body

$$\psi = U r \sin \theta + m \theta, \quad m = \frac{Q}{2\pi}$$

At stagnation point, $r = a$, $\theta = \pi$

$$\psi = m\pi$$

$$V_r = u = \frac{m}{a} \Rightarrow a = \frac{m}{u}$$

So the equation of streamline passing through the stagnation point is:

$$a\pi u = U r \sin \theta + a u \theta \Rightarrow r = \frac{a(\pi - \theta)}{\sin \theta}$$

b) At point (0, 3), $r = 3$, $\theta = \frac{\pi}{2}$

$$3 = \frac{a(\pi - \frac{\pi}{2})}{\sin(\frac{\pi}{2})} = \frac{\pi a}{2} \Rightarrow a = \frac{6}{\pi} = 1.91 \text{ m}$$

a) $m = a u = \left(\frac{6}{\pi}\right)(7) = 13.37 \text{ m}^2/\text{s}$

c) At point (4, 0), $r = \frac{4}{\cos \theta}$

$$\frac{4}{\cos \theta} = \frac{1.9(\pi - \theta)}{\sin \theta} \Rightarrow \theta = 47.8^\circ$$

$$h = 4 \tan \theta = 4 \tan(47.8^\circ) = 4.44 \text{ m}$$

d) $v^2 = V_r^2 + V_\theta^2 = u^2 \left(1 + 2 \frac{a}{r} \cos \theta + \frac{a^2}{r^2}\right)$

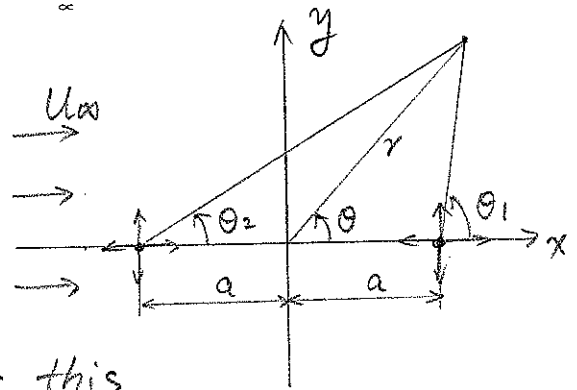
$$= 7^2 \left(1 + \frac{(2)(1.91)}{4 / \cos(47.8^\circ)} \cos(47.8^\circ) + \frac{1.91^2}{4^2 / \cos^2(47.8^\circ)}\right) = (8.67)^2$$

#11. Sketch the streamlines, especially the body shape, due to equal line sources $+m$ at $(-a,0)$ and $(+a,0)$ plus a uniform stream $U_\infty = ma$.

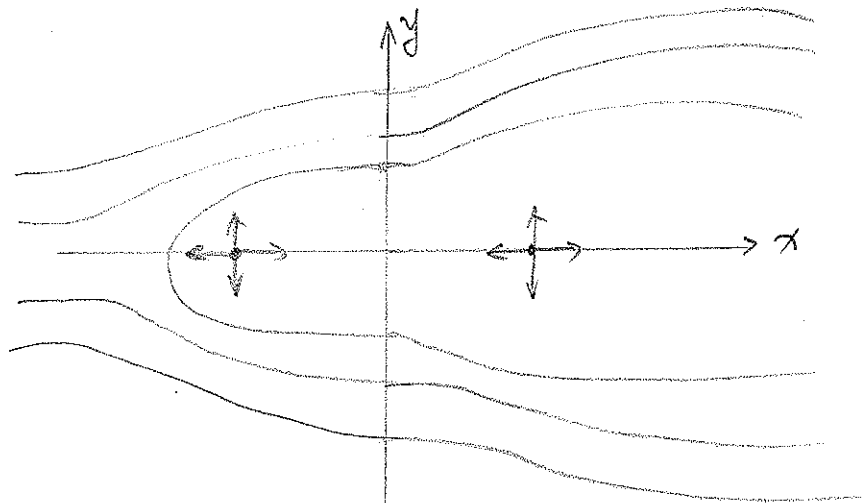
Solve: $\psi = \psi_{\text{uniform}} + \psi_{\text{two source}}$

$$= U_\infty r \sin\theta + m(\theta_1 + \theta_2)$$

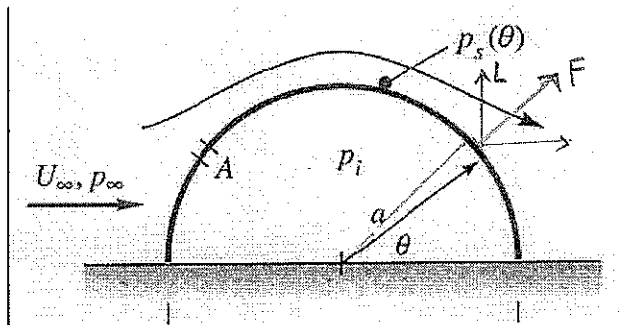
(superposition)



The corresponding streamlines for this flow field can be obtained by setting $\psi = \text{constant}$.



#12. A wind with U_∞ and p_∞ flows past a canopy. The canopy is modeled as a half-cylinder of radius a and length L into the paper as shown. The internal pressure is p_i . Using potential flow theory, derive an expression for the upward force on the canopy due to the difference between p_i and p_s .



Solve: On the surface, $U_\theta = -2U_\infty \sin\theta$

By Bernoulli equation

$$p_\infty + \frac{1}{2}\rho U_\infty^2 = p_s + \frac{1}{2}\rho U_s^2 = p_s + 2U_\infty^2 \sin^2\theta \rho$$

$$\Rightarrow p_s = \frac{1}{2}\rho U_\infty^2 (1 - 4\sin^2\theta) + p_\infty$$

$$dF = p dA = -(p_s - p_i) a d\theta \cdot L$$

$$dL = dF \sin\theta = -(p_s - p_i) \sin\theta a L d\theta$$

$$\therefore L = \int_0^\pi -aL \left[\frac{1}{2}\rho U_\infty^2 (1 - 4\sin^2\theta) + p_\infty - p_i \right] \sin\theta d\theta$$

$$= aL (p_i - p_\infty - \frac{1}{2}\rho U_\infty^2) \int_0^\pi \sin\theta d\theta - 2\rho U_\infty^2 aL \int_0^\pi \sin^3\theta d\theta$$

$$= 2aL (p_i - p_\infty - \frac{1}{2}\rho U_\infty^2) + 2\rho U_\infty^2 aL \cdot \frac{4}{3}$$

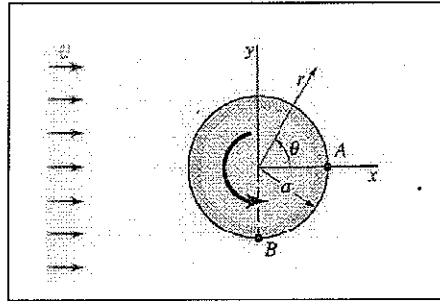
$$= 2La (p_i - p_\infty) + \frac{5}{3}\rho U_\infty^2 La$$

#13. A spinning cylinder is placed in a uniform irrotational and incompressible flow as shown below. For what angular velocity Ω will the stagnation point be located at:

a) point A

b) point B

Which case produces the greatest lifting force?



Solve: Adding a free vortex to velocity potential for the flow around a cylinder.

$$\phi = Ux \left(1 + \frac{a^2}{r^2}\right) \cos\theta + \frac{\Gamma}{2\pi} \theta$$

So, the tangential velocity V_θ on the surface of cylinder becomes

$$V_\theta = -\frac{\partial\psi}{\partial r} \Big|_{r=a} = -2U \sin\theta + \frac{\Gamma}{2\pi a}$$

For stagnation point, $V_\theta = 0$.

$$\Gamma = 4\pi a U \sin\theta$$

At point A: $\theta = 0 \Rightarrow \Gamma = 0$

At point B, $\theta = \frac{3}{2}\pi, \Rightarrow \Gamma = -4\pi a U$

$$\Omega = \frac{V_\theta}{a} = \frac{\Gamma}{2\pi a^2} = \frac{-4\pi a U}{2\pi a^2} = -\frac{2U}{a}$$

At point B: $F_y = -\rho U \Gamma = 4\pi a \rho U^2$, the greatest lifting force.