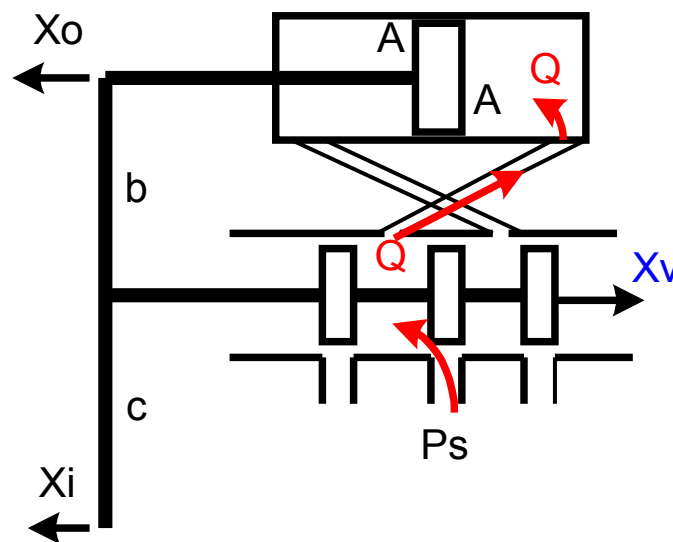


Name \_\_\_\_\_

1. A valve controlled actuator is shown below.  $X_i$  is the input and  $X_o$  is the output. Assume the fluid is incompressible and the valve is linear. Also assume no force is required to move the massless piston.
- (a) Label the flow variable and  $X_v$  and then write the corresponding equations for this system. Determine the transfer function relating  $X_i$  to  $X_o$ .
- (b) For a step input, how long will it take for the output to reach steady state?



For  $X_v$  and  $Q$  defined positive as shown, we get the following equations

$$Q = C_v X_v$$

$$Q - A\dot{X}_o = 0$$

Using superposition, the linkage equation is found to be

$$X_v = \frac{-c}{c+b} X_o + \frac{-b}{c+b} X_i$$

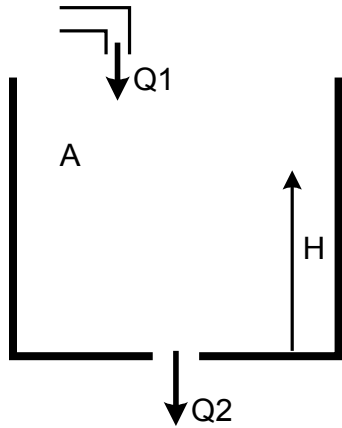
Laplace transforming and then eliminating  $Q$  and  $X_v$  gives

$$X_o(s) = -\frac{b}{c} \frac{1}{\tau s + 1} X_i(s)$$

$$\tau = \frac{(b+c)A}{cC_v}$$

The time to steady state is  $5\tau$ .

2. The water tank shown below has a constant input flow  $Q_1 = 0.0376$  m<sup>3</sup>/s. The flow through the hole at the bottom requires the orifice equation with  $C_d = 0.6$  and hole area  $A_o = 0.01$  m<sup>2</sup>. Gravity is  $g = 9.8$  m/s<sup>2</sup> and the density of the water is  $\rho = 1000$  kg/m<sup>3</sup>. The area of the tank is  $A = 0.50$  m<sup>2</sup>.



(a) Derive the differential equation for the height of the water in the tank.

$$Q_1 - Q_2 - A\dot{H} = 0$$

$$Q_2 = C_d A_o \sqrt{\frac{2}{\rho} P} = C_d A_o \sqrt{2gH}$$

Eliminating  $Q_2$  gives

$$A\dot{H} + C_d A_o \sqrt{2gH} = Q_1$$

Substituting for the given parameters gives

$$\dot{H} + 0.05313\sqrt{H} = 0.0752$$

(b) Determine the steady state height,  $H_{ss}$ , of the water in the tank.

$$0 + 0.05313\sqrt{H_{ss}} = 0.0752$$

Thus,

$$H_{ss} = 2 \text{ m}$$

(c) Obtain a linear differential equation by linearizing  $\sqrt{H}$  for values of  $H$  in the neighborhood of  $H_{ss}$ .

Linearizing in the neighborhood of  $H = 2$  gives

$$\sqrt{H} \approx \sqrt{2} + \frac{1}{2\sqrt{2}}(H - 2) = 0.3536H + 0.707$$

Thus,

$$\dot{H} + 0.05313(0.3536H + 0.707) = 0.0752$$

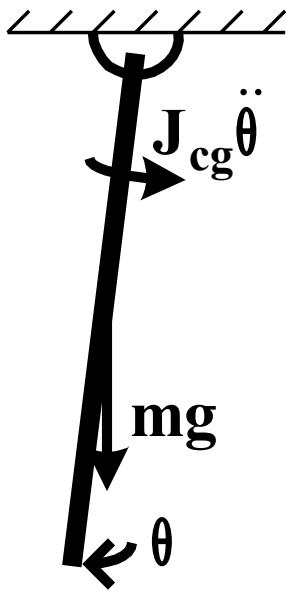
Or,

$$\dot{H} + 0.01879H = 0.03763$$

3. The uniform mass bar shown below swings like a pendulum. The length of the bar is  $L$  and the mass of the bar is  $M$ . Denote gravity by  $g$ . For the bar,  $J_{cg} = \frac{ML^2}{12}$ .

(a) Neglecting all friction, derive the differential equation for the angular position of the bar if it is released from some non-vertical position.

(b) Using the small angle approximation, estimate the oscillation frequency.



$$\left[ m \left( \frac{L}{2} \right)^2 + J_{cg} \right] \ddot{\theta} + mg \frac{L}{2} \sin \theta = 0$$

For small angles,  $\sin \theta \approx \theta$

Thus, the differential equation becomes

$$\ddot{\theta} + \omega_n^2 \theta = 0$$

The oscillation frequency  $\omega_n = \sqrt{\frac{3g}{2L}}$

## Useful Equations For Fluids

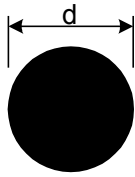
### Liquids

(Q m<sup>3</sup>/s, P Newtons/m<sup>2</sup> absolute or gauge, d m<sup>2</sup>, A & A<sub>v</sub> m<sup>2</sup>, L m)

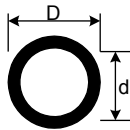
#### Resistance

$$P_u - P_d = RQ \quad \text{where}$$

$$R = \frac{128\mu L}{\pi d^4} \quad \text{Laminar flow through a circular tube, diameter } d$$



$$R = \frac{128\mu L}{\pi (D - d)^3 (3d - D)} \quad \text{Laminar flow between concentric tubes, diameters } d \text{ \& } D$$



For an orifice or turbulent flow in a tube:

$$P_u - P_d = \frac{\rho}{2C_d^2 A_o^2} Q|Q| \quad \text{or} \quad Q = C_d A_o \sqrt{\frac{2|P_u - P_d|}{\rho}} \text{sign}(P_u - P_d)$$

For a valve, use the  $C_d \approx 0.6$  for a sharp edged orifice.

$$\text{For turbulent flow in a tube use } C_d = \sqrt{\frac{d}{Lf}} \quad f = 0.3164\Re^{-0.25}$$

$$\Re = \frac{\rho \bar{u} d}{\mu} = \frac{4\rho Q}{\mu \pi d} \quad \text{which is the Reynolds Number}$$

#### Inertance

$$P_u - P_d = \frac{\rho L}{A} \dot{Q} \quad \text{or} \quad P_u - P_d = I\dot{Q}$$

#### Capacitance

$$Q_{in} - Q_{out} - \dot{V} = \frac{V}{\beta} \dot{P} \quad \text{or} \quad Q_{in} - Q_{out} = C\dot{P}$$